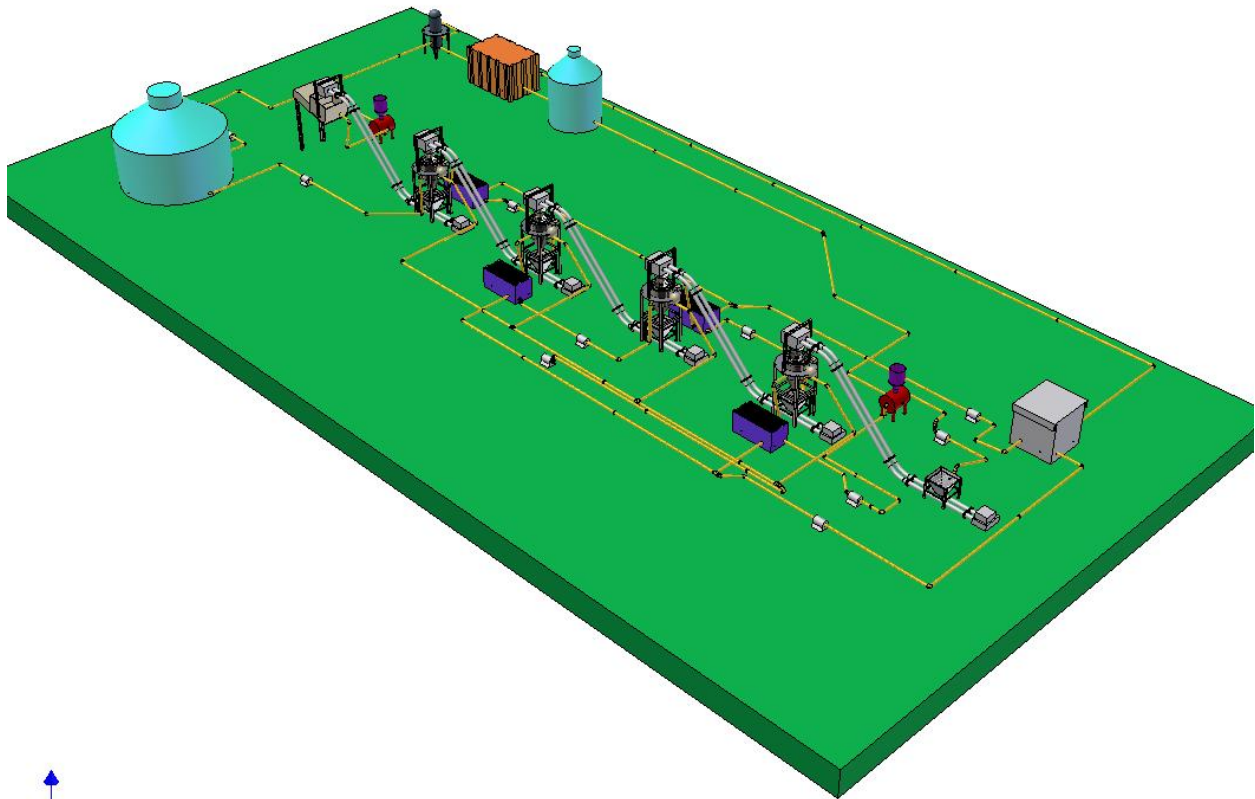




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GENOIL SAND DECONTAMINATION TECHNOLOGY (GSDT)





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DESCRIPTION

The Genoil Sand Decontamination Technology (GSDDT) is an innovative process designed to cleanse oil sands using minimal water and energy consumption thereby allowing the reclamation of refineries, well fields, waste pits, and beaches contaminated by petroleum.

Genoil Inc. was one of the first companies to enter this field and our revolutionary extraction and soil remediation methods are truly unique. Our process removes and reclaims oil from the sand and has little or no impact on the environment. We are the only company of our kind using this innovative process that is both efficient and environmentally friendly. There is no one at this time that is able to reclaim the oil while returning the sand to agricultural grade sand meeting bit dryness (lack of water in the sand) and contaminants such as oil and metals.

The process evolved from extensive experience acquired with earlier sand washing plants based on Genoil patented technologies. The technology presented here is the latest stage of development of this process featuring significant improvements such as: energy efficient steam cleaners, redesigned reactors, multiple dewatering stages, and an elutriation water purifying system.

To understand the significance of this breakthrough it is important to understand traditional tar sand technology. The process has changed little since the 1930's and the only commercial plants, located in Alberta, Canada, use a hot water steam process to release oil from the sand. The plants needed to upgrade the reclaimed oil are expensive (accounting for 90 percent of capital costs) and the process generates massive toxin-filled tailing ponds. These traditional plants are considered one of the world's worst air polluters and approval from the U.S. Bureau of Land Management for a conventional Canadian process plant in the United States is highly unlikely.



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GENERAL PROCESS DESCRIPTION AND SYSTEM CONFIGURATION

Process Description

With reference to the Process Flow Diagram that follows in the next section, sand is metered and fed to reactor No.1, where the decontamination process occurs in several steps.

1. Initially powerful steam jets extract and separate the bulk of hydrocarbons from the sand. A device guides the sand on a helical path exposing it to steam cleansing and also facilitating hydrocarbon removal.
2. Sand then falls through a rinsing section where water jets detach residual oil particles by way of vigorous agitation. Oil rises to the water surface and joins the froth that resulted from steam cleansing. A funnel-shaped weir confines the froth around an oil skimmer and also isolates inadvertently entrained sand particles. The skimmer conveys the froth to a decanter where oil is reclaimed for reuse. Furthermore, the water jets disperse other contaminants contained by sand, particularly dissolved solids, and forms a relatively diluted solution. Water emerging from the rinsing device flows upwardly through the reactor and then cascades into an adjacent gravity separator.
3. Meanwhile, sand descends to a solids-water separation zone and forms a blanket of controlled thickness. The sand layer acts as a barrier, blocking the migration of contaminants to the reactors disposed downstream. A specially designed conveyor dewateres and meters the sand in the lower portion of reactor No. 1. Relatively dry sand is then transferred to the steam-cleansing section of reactor No. 2, where the decontamination process is resumed. Due to removal of water from sand, the amount of dissolved contaminants reaching reactor No. 2 is further reduced.
4. From reactor No.2, sand is conveyed downstream and similarly processed through reactors Nos. 3, 4 and 5. Sand is thus rendered progressively cleaner until it meets environmental standards. Clean sand is finally transferred to a dewatering device where it is suitably dried and rendered transportable to disposal sites.
5. Vital to the decontamination process is a countercurrent flow of elutriation water through the reactors. Elutriation water is supplied from duly selected sources such as rivers or lakes and stored in a tank. When sand is being reclaimed for certain applications, elutriation water needs to contain a minor amount of dissolved solids. In such situations distilled water is the only alternative and is to be produced by way of reverse osmosis units. A limited amount of elutriation water is also supplied to the steam cleaners in order to form steam jets.



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6. After rinsing and diluting the contaminants in the reactor, elutriation water is diverted to a corresponding gravity separator. Oil particles are duly removed from the stream whereas dissolved solids and clay pass through the separator. Consequently dissolved solids, which are initially diluted in reactor No. 5, become increasingly concentrated as elutriation water moves upstream through the reactors.

7. The sand washing plant is designed to balance the amount of dissolved contaminants entering the reactors with the contaminants leaving them. A computer program maintains the concentration of contaminants in each reactor at preset levels for ensuring stable product quality. To this end the program calculates the amount of elutriation water needed in various situations and accordingly regulates the flow rate.

8. Upon completing the rinsing process in reactor No.1, elutriation water contains concentrated contaminants and is diverted to a purification system for recycling.

9. At first three clarification tanks disposed in parallel extract the fines. The clarifiers operate in conjunction with a floating arrangement that minimizes agitation in order to enhance the clarification process. Relatively clear water emerging from the clarifiers is further processed in a polishing oily-water separator designed to remove minute particles of oil that could not be separated by gravity. Elutriation water is then filtered and treated to meet the exacting requirements of the reverse osmosis unit. After desalting, the bulk of elutriation water is recycled to the storage tank whereas brine is pumped to a disposal well. As a result, the water consumption can be reduced by at least 50%. In certain situations it is economical to utilize reverse osmosis units disposed in series, an arrangement that maximizes the amount of water that can be recycled. In northern regions reducing the amount of cold water supplied from rivers also brings about important heat energy savings.

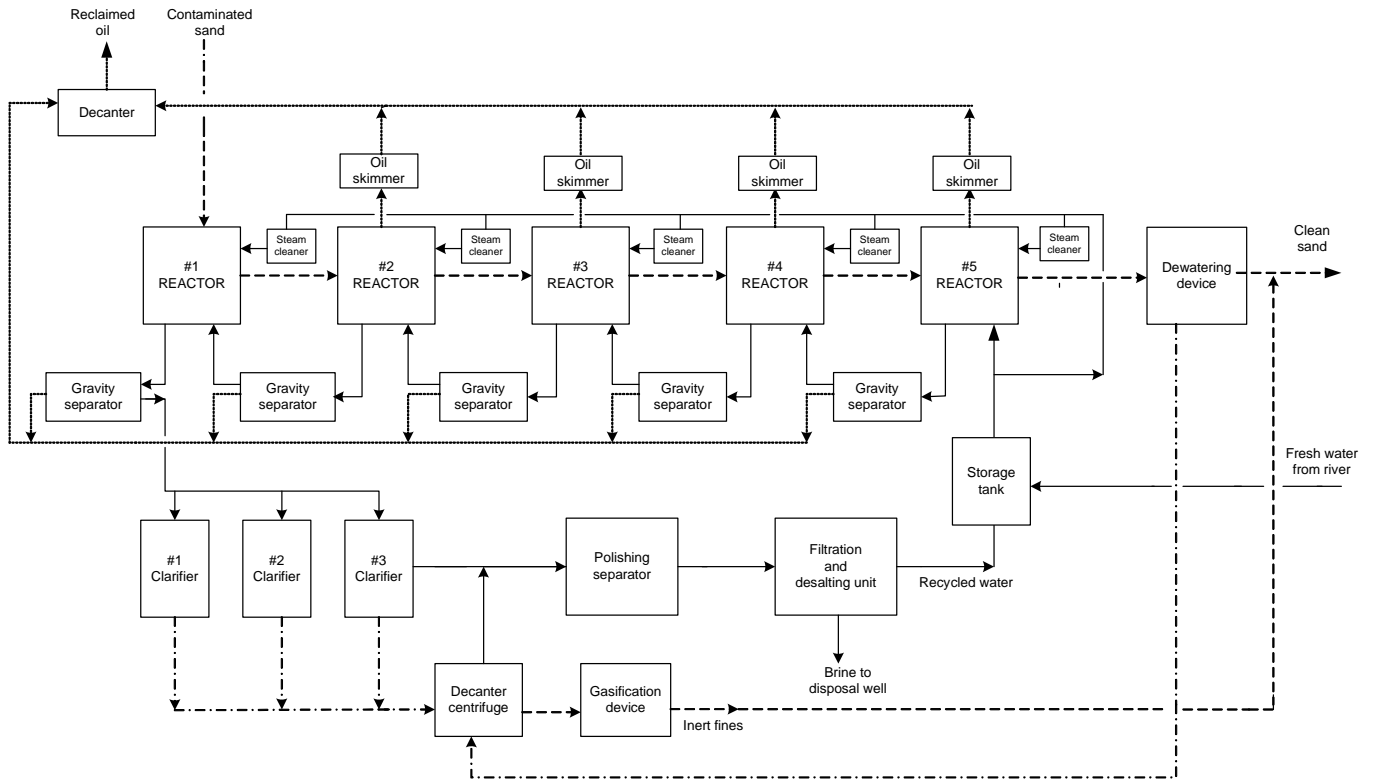
10. Fines originating from the clarifiers are further dewatered by means of a decanter centrifuge. Clean water overflowing from the centrifuge is redirected to the purification system and recycled. Cake accumulated in the centrifuge is processed with minimal emissions and energy consumption through a gasification device that eliminates traces of oil in order to render the fines suitable for disposal.



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GENOIL SAND DECANTAMINATION TECHNOLOGY (GSDT) PROCESS FLOW DIAGRAM

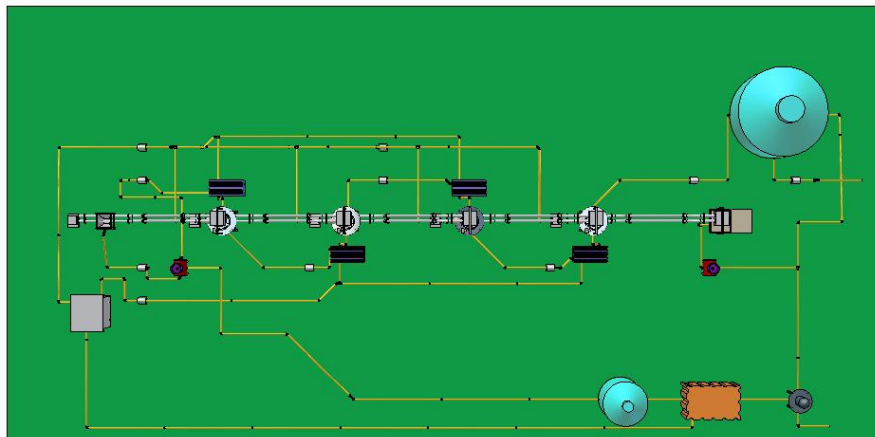
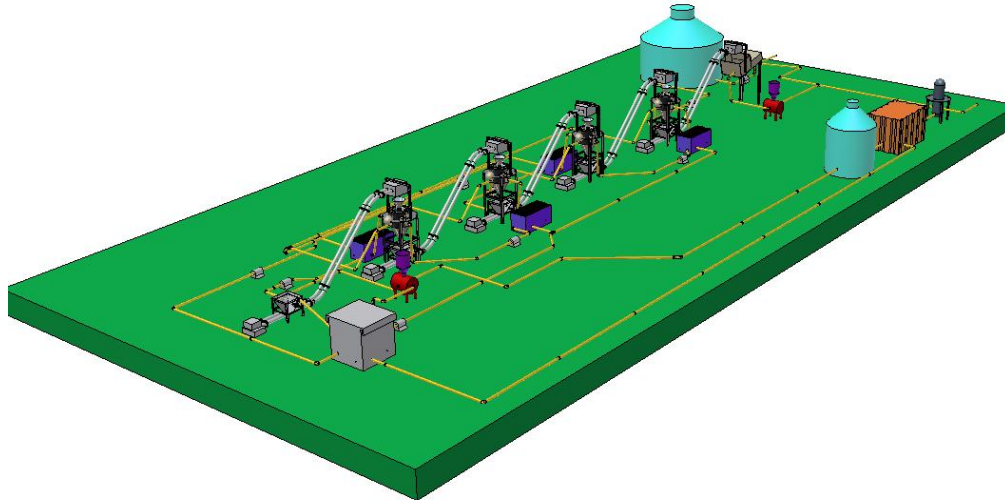
Figure 1





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3D DRAWINGS





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FIELD TESTING RESULTS

We have conducted two field tests by an **independent laboratory**, Maxxam Analytics Inc., on some of the components that produced impressive results. The next step in this evolution is to build a 2 cubic meter per hour portable unit for field testing.

The portable plant is designed to operate at a capacity of 2 cubic meters per hour, containing about 10 to 15% oil, 30% water by volume, TDS content: about 33000 mg/l (typical sea or produced water), clay: 5%, fines (silica) below 50 microns 5%. The plant is to be supplied with fresh water from river or lake with a TDS content of 200 mg/l. The Mass balance indicates a product with 10% water in sand by volume, a TDS content in the water of 300 mg/l (basically harmless TDS content, just like tap water) and a water consumption of 1100 to 1300 liters per hour depending on the rejection rate of the reverse osmosis unit (1300 liters at 70% rejection rate which is very conservative).

It should be noted that the mass balance was done for five reactors in order to minimize the water consumption and the size of the equipment. Initially, four reactors were intended, but the risk of significantly increased water consumption outweighed the savings resulting from using one less reactor. Instead, we opted for a basket centrifuge for clarification in order to save space, which is at a premium in a portable unit.

Another option is to use a 20 gpm capacity Crystal separator for the portable plant. Dimensions and weights related to capacities or at least to one capacity as an example: A 2 cubic meters per hour plant would fit in two 40 feet containers but precise dimensions and weights are not available at this time. Possible applications: The technology is devised to decontaminate any oil polluted sands and bring them to environmental standards in terms of oil content and salinity.

Minimum and maximum capacities of the system in the appropriate unit like cubic meters per hour: The maximum capacity of the plant is limited by the availability of fresh water which can be supplied to the system from rivers or lakes. The minimum capacity for practical purposes is 2 cubic meters of processed sand per hour.

A plant of 10 cubic metres per hour of processed sand would typically require 7 cubic meters per hour of fresh water. The water consumption is proportional to the amount of sand that is to be processed, and for a given amount of sand it could fluctuate by about +/- 5%.

Environmental impact:

One of the most impressive features of the process is how environmentally benign it is. We use no harsh chemicals, do not contaminate the soil we work with, and create no tailing ponds. Our method removes and recovers nearly all of hydrocarbons, producing clean saleable sand. We are able to reclaim the oil while returning the sand to near agricultural grade sand with the least amount of impact on the local environment, while using the least amount of natural resources like water and natural gas.



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PRINCIPAL FEATURES OF GENOIL SAND DECONTAMINATION TECHNOLOGY

- Produces Sand Quality Within Environmental Requirements (< 300 ppm Total Dissolved Solids)
- Moderate Capital and Operational Costs
- Moderate Energy Consumption (approximately 300 KW for a 10 m³/hour plant)
- Moderate Water Requirements Due To Recycling (approximately 7 m³/hour for a 10 m³/hour capacity plant)
- Maximum Capacity Limited Only by Availability of Water from Lakes or Streams (minimum system capacity 2 m³/hour)
- Can Use Sea Water for Cleaning Beach Sand
- Portable (2 m³/hour unit would require only two 40' containers for transporting)